

I. AMENDMENTS TO THE CLAIMS

Claim 1. (Previously Presented) An elimination process of fluorinated anionic surfactants from exhausted gaseous streams wherein the gaseous stream is put into contact with aqueous solutions having pH from 3.5 to 13.8, the aqueous solution density being lower than 1.05 g/cm³, wherein the concentration in the aqueous solution of the fluorinated anionic surfactant removed from the gaseous stream is lower than or equal to 70 ppm.

Claim 2. (Previously Presented) The process according to claim 1, wherein the anionic fluorinated surfactants are selected from perfluorinated carboxylic acids or derivatives thereof.

Claim 3. (Currently Amended) The process according to claim 1, wherein the contact between the gaseous stream and the aqueous ~~solutions~~ solution is carried out in a scrubber.

Claim 4. (Previously Presented) The process according to claim 3, wherein the scrubber is a filling up column.

Claim 5. (Previously Presented) The process according to claim 1, wherein the process operates in a discontinuous or a continuous way.

Claim 6. (Currently Amended) The process according to ~~claim 5~~ claim 3, wherein the process operates in the continuous way according to a method selected from the group consisting of:

- recycling the solution and recovering the surfactant at each recycle;
- recycling the solution until reaching a surfactant concentration of 70 ppm and then by treating a liquid phase to remove the surfactant;
- using in the scrubber fresh solution without recycle; and
- feeding a fresh aqueous solution aliquot and drawing from the scrubber an aliquot containing the anionic surfactants to be recovered.

Claim 7. (Currently Amended) The process according to ~~claim 5~~ claim 3, wherein when the process operates in the discontinuous way, the solution used in the scrubber is recycled until a surfactant concentration of 70 ppm is reached.

Claim 8. (Currently Amended) The process according to ~~claim 4~~ claim 6, wherein the surfactant is recovered from the aqueous solution flowing out from the ~~absorption column~~ scrubber by a method selected from the group consisting of:

- passing the solution on anionic exchange resins;
- using specific adsorbers for fluorinated surfactants;
- reverse osmosis units; and
- precipitation with ~~polivalent~~ polyvalent cation salts.

Claim 9. (Previously Presented) The process according to claim 8, wherein a strong anionic exchange resin is used.

Claim 10. (Previously Presented) The process according to claim 8, wherein the used specific adsorbers are selected from the group consisting of active carbon, aluminas, and silicas.

Claim 11. (Currently Amended) The process according to ~~claim 4~~ claim 6, wherein the ~~initial removal~~ aqueous solution from which the surfactant is recovered, and/or the recycle solution have a temperature in the range 5°C-40°C.

Claim 12. (Currently Amended) The process according to ~~claim 4~~ claim 3, wherein, in the scrubber, the ratio by weight among flow rates of the ~~feeding~~ aqueous solution and ~~feed gas~~ gaseous stream is from 2 to 20.

Claim 13. (Previously Presented) The process of claim 1, wherein the aqueous solution density is lower than 1.03 g/cm³.

Claim 14. (Previously Presented) The process of claim 1, wherein the concentration in the aqueous solution of the fluorinated anionic surfactant removed from the gaseous stream is lower than or equal to 60 ppm.

Claim 15. (Previously Presented) The process of claim 1, wherein the concentration in the aqueous solution of the fluorinated anionic surfactant removed from the gaseous stream is lower than 50 ppm.

Claim 16. (Previously Presented) The process of claim 2, wherein the anionic fluorinated surfactants are perfluorooctanoate in acid or salified form.

Claim 17. (Previously Presented) The process of claim 4, wherein the scrubber is one member selected from the group consisting of a structured column, a plate column and a spray column.

Claim 18. (Previously Presented) The process of claim 4, wherein the scrubber is the structured column.

Claim 19. (Previously Presented) The process of claim 11, wherein the temperature is in the range of 10°C-30°C.

Claim 20. (Previously Presented) The process of claim 12, wherein the ratio is from 4 to 15.